

ALERT! ALERT! CORRECTION TO LAST LECTURE

Suppose that source enters the up gradient end of a column

At a continuous concentration of $C_o=1000\text{mg/l}$

$K = 0.1 \text{ cm/sec}$

$dh = 10 \text{ cm}$

$dl = 100 \text{ cm}$

$\phi = 0.2$

Dispersivity $\alpha_x = 5 \text{ cm}$

what will the concentration be at 50 cm after 1000sec?

average linear velocity

$$\bar{v} = \frac{Kdh}{\phi dl} = \frac{0.1 \frac{\text{cm}}{\text{sec}}}{0.2} \frac{10\text{cm}}{100\text{cm}} = 0.05 \frac{\text{cm}}{\text{sec}}$$

distance traveled in 1000sec?

$$d = \bar{v}t = 0.05 \frac{\text{cm}}{\text{sec}} 1000 \text{ sec} = 50\text{cm}$$

By inspection we **expect** the concentration should be $0.5 \cdot C_o = 500\text{mg/l}$

But let's carry out the calculation

ALERT! ALERT! CORRECTION TO LAST LECTURE – EXCEL WAS CORRECT

$$\bar{v} = 0.05 \frac{\text{cm}}{\text{sec}} \quad D_x = \bar{v}\alpha + D^* = 0.05 \frac{\text{cm}}{\text{sec}} 5\text{cm} + 1 \times 10^{-10} \frac{\text{m}^2}{\text{sec}} \frac{10000\text{cm}^2}{1\text{m}^2} = 0.25 \frac{\text{cm}^2}{\text{sec}}$$

$$C = \frac{C_o}{2} \left(\operatorname{erfc} \left(\frac{x-vt}{2\sqrt{D_x t}} \right) + \exp \left(\frac{\bar{v}x}{D_x} \right) \operatorname{erfc} \left(\frac{x+vt}{2\sqrt{D_x t}} \right) \right)$$

Often this term is ignored because it is typically small, but we carry it through here.

$$C = \frac{1000 \frac{\text{mg}}{\text{l}}}{2} \left(\operatorname{erfc} \left(\frac{50\text{cm} - 0.05 \frac{\text{cm}}{\text{sec}} 1000\text{sec}}{2\sqrt{0.25 \frac{\text{cm}^2}{\text{sec}} 1000\text{sec}}} \right) + \exp \left(\frac{0.05 \frac{\text{cm}}{\text{sec}} 50\text{cm}}{0.25 \frac{\text{cm}^2}{\text{sec}}} \right) \operatorname{erfc} \left(\frac{50\text{cm} + 0.05 \frac{\text{cm}}{\text{sec}} 1000\text{sec}}{2\sqrt{0.25 \frac{\text{cm}^2}{\text{sec}} 1000\text{sec}}} \right) \right)$$

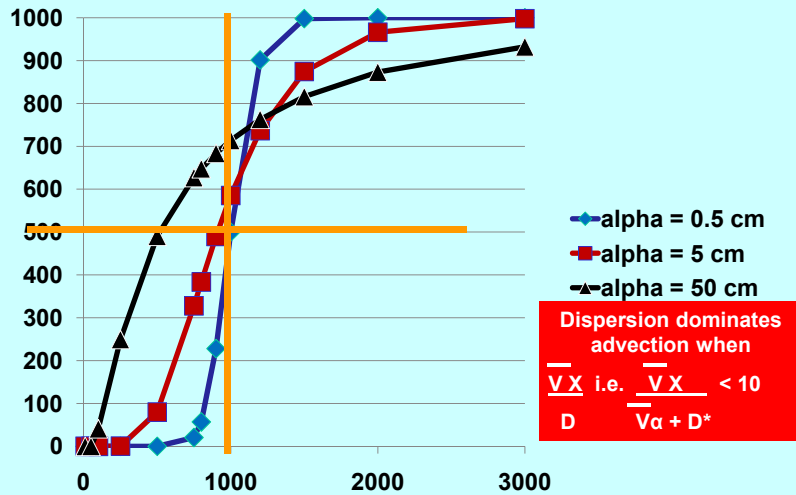
In this case including the second term provides a more accurate result

$$C = 500 \frac{\text{mg}}{\text{l}} \left(\operatorname{erfc} \left(\frac{50\text{cm} - 50\text{cm}}{31.62\text{cm}} \right) + \exp \left(\frac{2.5 \frac{\text{cm}^2}{\text{sec}}}{0.25 \frac{\text{cm}^2}{\text{sec}}} \right) \operatorname{erfc} \left(\frac{50\text{cm} + 50\text{cm}}{31.62\text{cm}} \right) \right)$$

C is greater than 500 at the average travel time distance because dispersion dominates velocity near the source

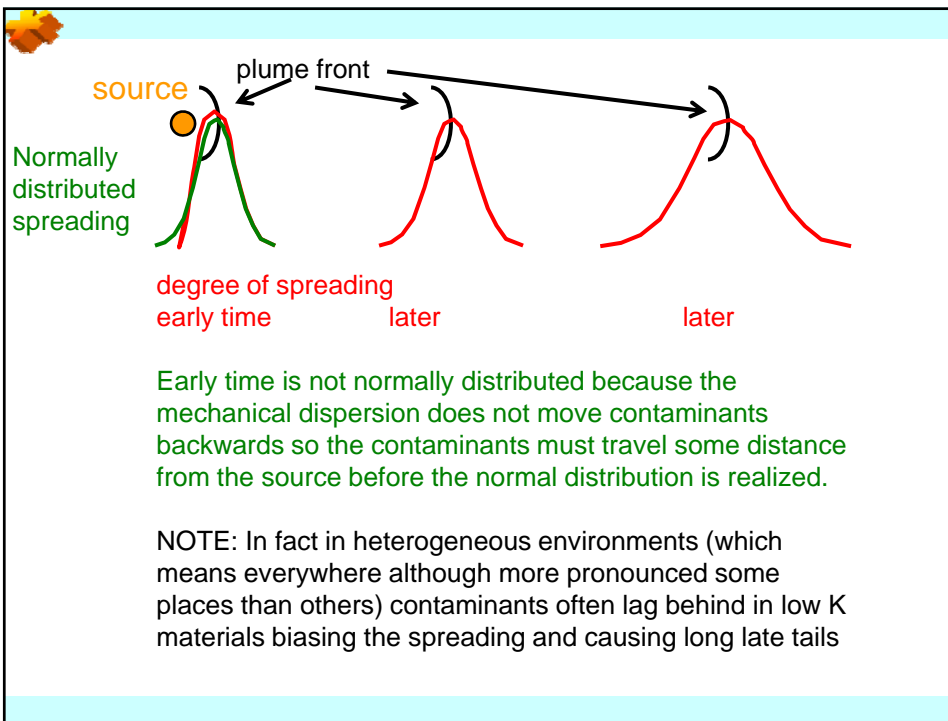
$$C = 500 \frac{\text{mg}}{\text{l}} (\operatorname{erfc}(0.0) + \exp(10)\operatorname{erfc}(3.1623)) = 500 \frac{\text{mg}}{\text{l}} (1.0 + 22026.46(7.743 \times 10^{-7})) = 585.3 \frac{\text{mg}}{\text{l}}$$

http://inside.mines.edu/~epoeter/_GW/22ContamTrans/C1d.xls



CONCLUSION DOES NOT CHANGE

The second term is important for calculating C @ early times near the source.



Suppose a source **continuously** enters that uniform flow field
 With an initial **concentration** of $C_o=1,000\text{mg/l}$

pause to consider relationship of mass and concentration

$$\text{Mass} = \text{Conc} * \text{Volume}$$

$$\text{Mass/Time} = \text{Conc} * \text{Velocity} * \text{Area} = \text{Conc} * Q \quad (Q \text{ is discharge})$$

$$\text{Mass} = \text{Conc} * Q * \text{Time}$$

Envision the source is submerged and
 emanates from a 0.5cm high x 1cm wide zone

pause to consider the character of the source geometry

$$v = 0.05 \text{ cm/sec}$$

$$\text{dispersivity } \alpha_x = 5 \text{ cm}$$

$$\text{dispersivity } \alpha_y = 1/5 \alpha_x$$

$$\text{dispersivity } \alpha_z = 1/10 \alpha_x$$

What will the concentration be at 50 cm
 directly down gradient after 1000sec?

pause to consider the coordinate system

$$\bar{v} = 0.05 \frac{\text{cm}}{\text{sec}}$$

$$D_x = \bar{v} \alpha_x + D^* = 0.05 \frac{\text{cm}}{\text{sec}} 5\text{cm} + 1 \times 10^{-10} \frac{\text{m}^2}{\text{sec}} \frac{10000\text{cm}^2}{1\text{m}^2} = 0.25 \frac{\text{cm}^2}{\text{sec}}$$

$$D_y = \bar{v} \alpha_y + D^* = 0.05 \frac{\text{cm}}{\text{sec}} 5\text{cm} \frac{1}{5} + 1 \times 10^{-10} \frac{\text{m}^2}{\text{sec}} \frac{10000\text{cm}^2}{1\text{m}^2} = 0.05 \frac{\text{cm}^2}{\text{sec}}$$

$$D_z = \bar{v} \alpha_z + D^* = 0.05 \frac{\text{cm}}{\text{sec}} 5\text{cm} \frac{1}{10} + 1 \times 10^{-10} \frac{\text{m}^2}{\text{sec}} \frac{10000\text{cm}^2}{1\text{m}^2} = 0.025 \frac{\text{cm}^2}{\text{sec}}$$

$$C(x, y, z, t) = \frac{C_o}{8} \left(\text{erfc} \left(\frac{x - \bar{v}t}{2\sqrt{D_x t}} \right) \right) \left(\text{erf} \left(\frac{y + \frac{Y}{2}}{2\sqrt{D_y \frac{x}{\bar{v}}}} \right) - \text{erf} \left(\frac{y - \frac{Y}{2}}{2\sqrt{D_y \frac{x}{\bar{v}}}} \right) \right) \left(\text{erf} \left(\frac{z + \frac{Z}{2}}{2\sqrt{D_z \frac{x}{\bar{v}}}} \right) - \text{erf} \left(\frac{z - \frac{Z}{2}}{2\sqrt{D_z \frac{x}{\bar{v}}}} \right) \right)$$

$$2\sqrt{D_x t} = 2 \sqrt{0.25 \frac{\text{cm}^2}{\text{sec}} 1000\text{sec}} = 31.62\text{cm}$$

$$2\sqrt{D_y \frac{x}{\bar{v}}} = 2 \sqrt{0.05 \frac{\text{cm}^2}{\text{sec}} \frac{50\text{cm}}{0.05 \frac{\text{cm}}{\text{sec}}}} = 14.14\text{cm}$$

$$2\sqrt{D_z \frac{x}{\bar{v}}} = 2 \sqrt{0.025 \frac{\text{cm}^2}{\text{sec}} \frac{50\text{cm}}{0.05 \frac{\text{cm}}{\text{sec}}}} = 10\text{cm}$$

$$C(x, y, z, t) = \frac{C_0}{8} \left(\operatorname{erfc} \left(\frac{x - \bar{v}_x t}{2\sqrt{D_x t}} \right) \right) \left(\operatorname{erf} \left(\frac{y + \frac{Y}{2}}{2\sqrt{D_y \frac{x}{\bar{v}}}} \right) - \operatorname{erf} \left(\frac{y - \frac{Y}{2}}{2\sqrt{D_y \frac{x}{\bar{v}}}} \right) \right) \left(\operatorname{erf} \left(\frac{z + \frac{Z}{2}}{2\sqrt{D_z \frac{x}{\bar{v}}}} \right) - \operatorname{erf} \left(\frac{z - \frac{Z}{2}}{2\sqrt{D_z \frac{x}{\bar{v}}}} \right) \right)$$

$$2\sqrt{D_x t} = 2\sqrt{\frac{0.25 \frac{\text{cm}^2}{\text{sec}} \cdot 1000 \text{sec}}{}} = 31.62 \text{cm}$$

$$2\sqrt{D_y \frac{x}{\bar{v}}} = 2\sqrt{\frac{0.05 \frac{\text{cm}^2}{\text{sec}} \cdot \frac{50 \text{cm}}{0.05 \frac{\text{cm}}{\text{sec}}}}{}} = 14.14 \text{cm}$$

$$2\sqrt{D_z \frac{x}{\bar{v}}} = 2\sqrt{\frac{0.025 \frac{\text{cm}^2}{\text{sec}} \cdot \frac{50 \text{cm}}{0.05 \frac{\text{cm}}{\text{sec}}}}{}} = 10 \text{cm}$$

$$x - \bar{v}_x t = 50 \text{cm} - 0.05 \frac{\text{cm}}{\text{sec}} \cdot 1000 \text{sec} = 0 \text{cm}$$

$$y + \frac{Y}{2} = 0 + \frac{1 \text{cm}}{2} = 0.5 \text{cm} \quad y - \frac{Y}{2} = 0 - \frac{1 \text{cm}}{2} = -0.5 \text{cm}$$

$$z + \frac{Z}{2} = 0 + \frac{0.5 \text{cm}}{2} = 0.25 \text{cm} \quad z - \frac{Z}{2} = 0 - \frac{0.5 \text{cm}}{2} = -0.25 \text{cm}$$

$$C = \frac{1000 \frac{\text{mg}}{\text{l}}}{8} \left(\operatorname{erfc} \left(\frac{0}{31.62 \text{cm}} \right) \right) \left(\operatorname{erf} \left(\frac{0.5 \text{cm}}{14.14 \text{cm}} \right) - \operatorname{erf} \left(\frac{-0.5 \text{cm}}{14.14 \text{cm}} \right) \right) \left(\operatorname{erf} \left(\frac{0.25 \text{cm}}{10 \text{cm}} \right) - \operatorname{erf} \left(\frac{-0.25 \text{cm}}{10 \text{cm}} \right) \right)$$

$$C = 125 \frac{\text{mg}}{\text{l}} (\operatorname{erfc}(0)) (\operatorname{erf}(0.0354) - \operatorname{erf}(-0.0354)) (\operatorname{erf}(0.025) - \operatorname{erf}(-0.025))$$

$$C = 125 \frac{\text{mg}}{\text{l}} (1) (0.0399 - (-0.0399)) (0.0282 - (-0.0282)) \quad C = 0.56 \frac{\text{mg}}{\text{l}}$$

What do you make of the concentration relative to the C we obtained for the slug source?

How much mass enters the system in 1000sec? $M = CQT = CAV_D T$

How would you go about developing a contour map of the plume?

If you did not know the dispersivities, how could you use this equation to estimate them?

How might you set up the problem if 8g/d arrived at the water table over a 1m² area in an aquifer with the properties and conditions used for the example?

What do you make of the concentration relative to the C we obtained for the slug source?
 The slug source concentration at 50cm and 1000sec is 2 orders of magnitude higher. This is intuitively reasonable. The slug added 1000mg at time zero.

How much mass enters the system in 1000sec? $M = CQT = CAV_D T$
 With the continuous source we have 1000mg/l entering an area of 0.5cm² for 1000sec at a Darcy velocity of 0.01cm/sec so the mass is lower and mass that entered later has not had the chance to travel far.

$$M = \text{Conc Area Velocity}_{\text{Darcy}} \text{Time}$$

$$\text{Total Mass} = \frac{1000 \text{mg}}{\text{liter}} * \frac{1 \text{liter}}{1000 \text{cm}^3} * 0.5 \text{cm}^2 * \frac{0.01 \text{cm}}{\text{sec}} * 1000 \text{sec} = 5 \text{mg}$$

On the other hand all the mass for the slug case has been dispersing for the full 1000sec.

How would you go about developing a contour map of the plume?
 For a given point in time calculate C at many x,y,z values then map then and contour them

If you did not know the dispersivities, how could you use this equation to estimate them?
 Collect concentration data by sampling water in the field then create a contour map using different values of dispersivity until a good match is obtained. There are some automated techniques for calibration that we will not go into here.

How might you set up the problem if 8g/d arrived at the water table over a 1m² area in an aquifer with the properties and conditions used for the example?
 Use formula for 2D downward spreading with a small Z, perhaps 0.0001 cm, and Y=100cm. The formula assumes the Q is the area of the source * DarcyV = 0.01cm² * 0.01cm/sec
 So to get 8g/d Co needs to be = $M / (\text{Area Velocity}_{\text{Darcy}} \text{Time}) =$

$$\text{Concentration} = 8000 \text{mg} / \left(0.01 \text{cm}^2 * \frac{0.01 \text{cm}}{\text{sec}} * 86400 \text{sec} \right) = \frac{926 \text{mg}}{\text{cm}^3} \frac{1 \text{liter}}{1000 \text{cm}^3} = \frac{9.26 \text{mg}}{\text{liter}}$$

For a material with a half-life of 12 yrs, how much is left after 40 yrs? (Hint figure it as a % of initial mass)

$$N = N_0 e^{(-\lambda t)} \quad \lambda = \frac{0.693}{T_{\frac{1}{2}}}$$

$$\lambda = \frac{0.693}{T_{\frac{1}{2}}} = \frac{0.693}{12 \text{ yrs}} = 0.05775 \text{ yrs}^{-1}$$

$$N = N_0 e^{(-\lambda t)}$$

$$N = 1 * e^{(-0.05775 \text{ yrs}^{-1} * 40 \text{ yrs})} = 0.099$$

or about 10%

It is often said that material is essentially gone after 7 half-lives. How much is left then?

$$N = N_0 e^{(-\lambda t)} \quad \lambda = \frac{0.693}{T_{\frac{1}{2}}}$$

$$\lambda = \frac{0.693}{T_{\frac{1}{2}}} = \frac{0.693}{1 \text{ unit}} = 0.693 \text{ units}^{-1}$$

$$N = N_0 e^{(-\lambda t)}$$

$$N = 1 * e^{(-0.693 \text{ units}^{-1} * 7 \text{ units})} = 0.0078 \sim 0.008$$

or less than 1%

What is the Retardation Coefficient for a site with

$$K_d = 0.01 \frac{\text{ml}}{\text{mg}}$$

effective porosity of 0.3
particle density of 2.65 g/cc

$$R = \frac{V_{\text{water}}}{V_{\text{contaminant}}} = \left(1 + \frac{\rho_b}{\phi_e} K_d \right)$$

$$\rho_b = (1 - 0.3) * 2.65 \frac{\text{g}}{\text{cc}} \frac{1000 \text{mg}}{\text{g}} \frac{1 \text{cc}}{1 \text{ml}} = 1855 \frac{\text{mg}}{\text{ml}}$$

$$R = \frac{V_{\text{water}}}{V_{\text{contaminant}}} = \left(1 + \frac{\rho_b}{\phi_e} K_d \right)$$

$$R = \left(1 + \frac{1855 \frac{\text{mg}}{\text{ml}}}{0.3} 0.01 \frac{\text{ml}}{\text{mg}} \right) = 62.8 \sim 63$$

What is the Retardation Coefficient for a site with

Ground water velocity = 0.05 cm/sec

Contaminant velocity = 0.0009 cm/sec

$$R = \frac{V_{\text{water}}}{V_{\text{contaminant}}} = \left(1 + \frac{\rho_b}{\phi_e} K_d \right)$$

$$R = \frac{V_{\text{water}}}{V_{\text{contaminant}}} = \left(1 + \frac{\rho_b}{\phi_e} K_d \right)$$

$$R = \frac{V_{\text{water}}}{V_{\text{contaminant}}} = \frac{0.05 \frac{\text{cm}}{\text{sec}}}{0.0009 \frac{\text{cm}}{\text{sec}}} = 55.56 \sim 56$$